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DPM flow pattern of LHD in underground mines with different ventilation conditions

R. Morla^{*}, S. Karekal and A. Godbole

School of Civil, Mining, and Environmental engineering, University of Wollongong, Australia

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Keywords	Abstract
-	Diesel-operated Load Haul Dumper (LHD) vehicles are commonly used in underground
Coal Mines	coal mines. Despite their value as utility vehicles, the main drawback of these vehicles is
	that they generate diesel particulate matter (DPM), a known carcinogenic agent. In this
DPM	work, an attempt is made to model DPM flows generated by LHDs in an underground
	coal mine environment for different DPM flow and intake air flow directions. The field
Diesel-Operated LHD	experiments are conducted and used to validate the computational fluid dynamics (CFD)
	models and used to map the DPM flow patterns. The results obtained show that if DPM
CFD Simulation	and the intake air co-flow (flow in the same direction), DPM is confined predominantly
	in the middle of the roadway. To the contrary, if the DPM and intake air counter-flow
	(flow in the opposite directions), the DPM spread occurs throughout the entire
	cross-section of the roadway. In the latter case, the operator will be more susceptible to
	exposure to high concentrations of DPM. Overall, the DPM concentration decreases
	with an increase in the intake air velocities. For co-flow for intake air velocities of 2 m/s,
	3 m/s, and 4 m/s, the DPM concentrations at 50 m downstream of the vehicles are 39 $(3^3 2^2 + 3^3 2^2)$
	$\mu g/m^3$, 23 $\mu g/m^3$, and 19 $\mu g/m^3$, respectively. The DPM concentration is also influenced
	by the DPM temperature at the source. For the DPM temperatures of 30 °C, 40 °C, 50
	°C, and 60 °C, the DPM concentrations at 50 m downstream of the source are 43 μ g/m ³ ,
	$34 \ \mu g/m^3$, $12 \ \mu g/m^3$, and $9 \ \mu g/m^3$, respectively.

1. Introduction

Diesel-operated LHD/Utility vehicles are commonly used in underground mines for loading and transportation of coal, ore, waste rock, and materials. These machines are efficient to reduce manpower, and improve productivity and safety. LHDs are generally operated at a speed of 20 to 30 km/h. The dimensions of an LHD are as follow: a length between 8 and 15 m, a width between 2.5 and 3.5 m, and a weight between 20 and 75 tons [1]. Each LHD consists of the front and back parts connected by articulated points. Each section of the unit has rubber wheels that are not steerable. Breaks, bucket, and steering are operated by the hydraulic system. These machines can operate by both the manual and the automatic systems.

The primary concern with these vehicles is the generation of diesel particulate matter (DPM), causing adverse health effects on the operators after a prolonged exposure. DPM is a by-product of an incomplete combustion of fuel in a diesel engine. These particles have a solid core mainly consisting of elemental carbon (EC) that is surrounded by organic carbon (OC). These two are cumulatively known as the total carbon (TC) [2]. Various research works [3] have concluded that exposure to diesel exhausts can cause cancer in humans.

As per Australian coal mine regulations, the maximum allowable 8-hour time-weighted average exposure to EC that is expelled from a diesel engine is 0.1 mg/m^3 [4-6].

Kan Corresponding author: ramsiit99@gmail.com (R. Morla).

To limit the DPM exposure to safe levels for the mine personnel, and to design effective DPM control strategies, comprehensive mapping of DPM near LHD is required for different flow conditions. This paper outlines a study of the DPM flow patterns near a diesel-powered LHD using computational fluid dynamics (CFD) simulations validated against the field experimental data. The field experiments were conducted in two stages using an Airtec real-time DPM monitoring instrument. In stage 1, the DPM concentration was monitored when the DPM and air intake flew in the same direction. In stage 2, the DPM and intake air flew in the opposite directions. For each stage, CFD simulation studies were carried out with different intake air velocities and DPM temperatures.

2. Materials and methods

2.1. Details of experimental mine and field experiment

To study the DPM flow pattern generated by LHD/Loader/Utility vehicles, field experiments were conducted in one of the coal mines of Coal India Limited. The mine has two 'depillaring' panels with continuous miners, one longwall panel, and a few development sections. The mine has five intake airways and two return air shafts, and the ventilation system of the mine is operated by two axial flow fans. To ensure that there was no DPM in the intake air, the field experiments

were conducted in an isolated intake airway. The air flow was controlled by a regulator located at the return side of the airway. A calibrated Airtec real-time DPM monitor was used for this field study. During the experiments, the flow rate of the instrument was adjusted to $2.83 \times 10-5$ m³/s (1.7 L per min). In this work, EC was considered as a DPM. In stage 1 of the experiments, the DPM source was placed such that the ventilation (intake) air and the DPM-laden 'smoke' flew in the same direction. In stage 2, the ventilation air and LHD smoke flew in the opposite directions. In these field studies, the test vehicle was a 150 kW LHD equipped with DPM filters and run in a 'no-load' condition.

2.2. Stage 1: DPM and ventilation air flow in same direction

In stage I, the experimental arrangement is such that the LHD exhaust smoke and the intake air flow in the same direction (co-flow), as shown in Figure 1. The DPM samples were collected downstream of LHD. Three sampling stations located at 2 m, 5 m, and 10 m from the vehicle were selected. Figure 1 shows the location of LHD and sampling stations. Each station had nine sampling points arranged in three rows (top, center, and bottom) and three columns (left, middle, and right). Figure 2 shows the location of sampling points in mine gallery.



Figure 1. Experiment stage 1: location of sampling stations and sampling points.



Figure 2. Details of sampling points in an experimental gallery.

2.3. Stage 2: DPM and ventilation air flow in opposite directions

In the stage 2 experiments, the LHD exhaust is arranged such that the smoke is directed opposite to the ventilation air flow. The DPM samples were collected downstream side of the LHD. In this case, the DPM samples were collected around LHD, and also at 6 m, 10 m, and 20 m downstream of LHD at a height of 1.2 m from the floor. Figure 3 shows the location and details of the sampling points. Three samples were collected at the 6 m sample station, and one sample was collected at the middle of the roadway at the 10 m and 20 m sample stations. During this experiment, the air flow in the experimental gallery was 32.4 m^3/s .



Figure 3. Stage 2: location of sampling stations and sampling points; top view.

2.4. CFD modelling

Numerical modelling studies with CFD have been used in the mining industry to solve various critical ventilation issues. Morla et al. (2013 and 2014) [7, 8] have used CFD to study inertisastion options to control the spontaneous combustion of coal for blasting gallery panels. Balusu (1993) [9] has conducted CFD modelling to design dust scrubber. Tanguturi and Balusu (2014) [10] used CFD modelling investigations to control methane flow and distribution in the back side of the supports near the tail gate. Tanguturi and Balusu (2015) [11] used the CFD modelling simulation studies to understand the longwall goaf gas flow strategies.

Hua et al. (2012) [12] investigated methane distribution flow pattern from adjacent coal seams of a longwall panel into the goaf with CFD. Ting (2005) [13] used CFD modelling simulations to simulate the longwall goaf gas flow behavior with respect to panel orientation, location of inertisation injection points, and location of goaf drainage holes. Ting and Wang (2013) [14] used the CFD modelling investigations with different air velocity flow rates at longwall face to simulate the gas and respirable dust particles.

Morla et al. (2017 and 2018) [15, 16] carried out basic CFD simulations of DPM flows generated by diesel-operated man-riding vehicles in coal mines. Similar CFD modelling studies have been conducted for metal mines for 30 kW stir skid loader (Zheng et al., 2011a, 2011b, Zheng et al., 2015a, 2015b) [17-20]. In the present work, we presented simulations of DPM generated by a diesel-operated LHD/Loader/Utility vehicle in a coal mine. The commercially available CFD package ANSYS Fluent (version 19.1) was used. The CFD simulations were carried out in the sequence of steps outlined in the following paragraphs.

2.4.1. Construction of computational domain and mesh

The computational domain is a 70 m long tunnel with a rectangular cross-section (width of 6 m, height of 2.7 m). A CAD model of an LHD vehicle was designed and imported into the computational domain. The location of the exhaust was at the rear end of LHD. The exhaust flow was a mixture of DPM and air. Figure 4 (a) shows the CAD model representing the vehicle, and Figure 4 (b) shows the experimental gallery with LHD. Figure 5 (a) shows the mesh generated for the complex surfaces of the vehicle, and (b) shows the details of the computational domain and mesh made up of about half-million computational cells. Finer cells were used to capture the details of the flow in regions such as small gaps and adjacent to solid surfaces.



a. LHD-CAD model.

b. Experimental gallery with LHD.



Figure 4. CFD model of man riding vehicle and experimental gallery.

Surface mesh of LHDb.Surface mesh of LHD & galleryFigure 5. (a) Meshed LHD, (b) Meshed gallery with LHD.

2.4.2. Setting up flow conditions

a.

The boundary conditions of the model were considered as the intake air velocity of 2 m/s and the 300 K temperature. The velocity of DPM was considered as 2 m/s at 323 K. DPM was considered as a pseudo-gas, and chemical reactions and collisions were not considered. The Boussinesq approximation was invoked to simulate the buoyancy effects and the standard k- ε model to simulate the turbulence.

2.4.3. Governing equations

Air flow in the tunnel was treated as a turbulent flow. To model turbulence, the Reynolds-Averaged Navier-Stokes equation was used. In Reynolds averaging, the solution variables in the exact Navier-Stokes equations consist of time-averaged and fluctuated components for velocity components [21].

$$u_i = \bar{u}_i + u_i$$
 (1)

where \bar{u}_i and u_i are the mean and fluctuating velocity components (*i* = 1, 2, 3).

The Reynolds-averaged Navier-Stokes (RANS) equation was obtained by substituting time and average velocity in the momentum equation:

$$\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x_i} \left(\rho u_i \right) = 0 \tag{2}$$



 $\frac{\partial}{\partial x}(\rho u_{i}) + \frac{\partial}{\partial x_{j}}(\rho u_{i}u_{j}) = -\frac{\partial p}{\partial x_{i}} + \frac{\partial}{\partial x_{j}}\left[\mu\left(\frac{\partial u_{i}}{\partial x_{j}} + \frac{\partial u_{j}}{\partial x_{i}} - \frac{2}{3}\delta_{ij}\frac{\partial u_{l}}{\partial x_{l}}\right)\right] + (3)$ $\frac{\partial}{\partial x_{j}}\left(-\rho\overline{u_{i}}^{*}u_{j}^{*}\right)$

where $-\rho u_i^{\ }u_j^{\ }$ is the Reynolds stress, which can be solved using the Boussinesq hypothesis and Reynolds stress models (RSMs). In the Boussinesq hypothesis, the Reynolds stress is related to the mean velocity gradient [21]:

$$-\rho \overline{u_i' u_j'} = \mu_t \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) - \frac{2}{3} \left(\rho k + \mu_t \frac{\partial u_k}{\partial x_k} \right) \delta_{ij}$$
(4)

To determine the turbulent viscosity, μ_t , the k- ε model was used.

$$\mu_t = \rho C_\mu \frac{k^2}{\varepsilon} \tag{5}$$

where C_{μ} is a constant, k is the turbulence kinetic energy, and ε is the dissipation rate of k. The turbulent heat transport is modelled using the concept of Reynolds analogy to turbulent momentum transfer. The modelled energy equation is as follows:

$$\frac{\partial}{\partial t} (\rho E) + \frac{\partial}{\partial x_{i}} \left[u_{i} (\rho E + p) \right] = \frac{\partial}{\partial x_{j}} \left[\left(k + \frac{c_{p} \mu_{i}}{\sigma_{k}} \right) \frac{\partial T}{\partial x_{j}} + u_{i} (\tau_{ij})_{eff} \right] + S_{h}$$
(6)

where *k* is the thermal conductivity, *E* is the total energy, and $(\tau_{ij})_{eff}$ is the deviatoric stress tensor, defined as:

$$\left(\tau_{ij}\right)_{eff} = \mu_{eff} \left(\frac{\partial u_j}{\partial x_i} + \frac{\partial u_i}{\partial x_j}\right) - \frac{2}{3} \mu_{eff} \frac{\partial u_k}{\partial x_k} \delta_{ij} \qquad (7)$$

The standard k- ε model is based on the model transport equations k and ε . The model transport equation for k was derived from the exact equation, while the model transport equation for ε was obtained using physical reasoning, and bears little resemblance to its mathematically exact counterpart.

In the derivation of the $k-\varepsilon$ model, the assumption is that the flow is fully turbulent, and the effect of molecular viscosity is negligible. As the mine air is considered as fully turbulent flow, the $k-\varepsilon$ model is valid for mine air.

The turbulent kinetic energy, k, and its rate of dissipation, ε , are obtained from the following governing equations [21]:

$$\frac{\partial}{\partial t} (\rho k) + \frac{\partial}{\partial x_{i}} (\rho k u_{i}) = \frac{\partial}{\partial x_{j}} \left[\left(\mu + \frac{\mu_{t}}{\sigma_{k}} \right) \frac{\partial k}{\partial x_{j}} \right] + G_{k} + G_{b} - \rho \varepsilon - Y_{M} + S_{k}$$

$$(8)$$

$$\frac{\partial}{\partial t}(\rho\varepsilon) + \frac{\partial}{\partial x_{i}}(\rho\varepsilon u_{i}) =
\frac{\partial}{\partial x_{j}} \left[\left(\mu + \frac{\mu_{i}}{\sigma_{\varepsilon}} \right) \frac{\partial \varepsilon}{\partial x_{j}} \right] +
C_{1\varepsilon} \frac{\varepsilon}{K} (G_{k} + C_{3\varepsilon}G_{b}) - C_{2\varepsilon} \rho \frac{\varepsilon^{2}}{K} + S_{\varepsilon}$$
(9)

where G_b is the generation of turbulent kinetic energy due to buoyancy, and G_k is the production of turbulent kinetic energy due to the mean velocity gradient.

To conduct the DPM investigations in a mine gallery, a 'species transport model' was used. ANSYS fluent predicts the local mass fraction of each species, Y_i , though the solution of a convection-diffusion equation for the i^{th} species. The conservation equation takes the following general form:

$$\frac{\partial}{\partial t} (\rho Y_i) + \Delta (\rho \vec{v} Y_i) = -\Delta \vec{J}_i + R_i + S_i$$
(10)

3. Results and discussions CFD simulations and field experiments

3.1. Stage 1: DPM and ventilation air flow in same direction (co-flow)

Figure 6 shows the results of the CFD simulations in isometric view when DPM and air flow are in the same direction (co-flow). A high DPM concentration is observed in the middle of the gallery. At 50 m downstream of the vehicle, the DPM particles are seen to spread over most of the middle gallery.

Figure 7 shows the contours of the DPM concentration at 2 m, 5 m, and 10 m downstream of the vehicle. In Figure 7 (a), a high DPM concentration is observed in the middle of the roadway. Figure 7 (b) shows the maximum concentration in the middle of the gallery, and a negligible concentration can be observed at the left and right sides of the roadways. Figure 7 (c) shows that the DPM flow move towards the roof of the roadway; DPM concentration at the center of the roadway is 70 μ g/m³, and low concentrations are observed at the left and right sides of the roadway.

Table 1 compares the field measurements with the CFD simulation results of the DPM concentration at the three sampling stations downstream of the vehicle. It can be observed that the simulated results are in a fair agreement with the measured data in most cases. Some discrepancies between the simulated and the measured results can be due to the unevenness in the gallery wall surfaces that were not considered while modelling. Overall, the difference varies from -17% to +21%.



Figure 6. DPM flow pattern for co-flow-isometric view.



a. DPM concentration at 2 m downstream of the vehicle.



b. DPM concentration at 5 m downstream of the vehicle.

Figure 7. EC concentration at 2 m, 5 m, and 10 m downstream of the vehicle.

0.000

			At sample	e station	2 m (µg	g/m ³)			
	Top row			Middle row			Bottom row		
Sample point	ER	SR	Difference, %	ER	SR	Difference, %	ER	SR	Difference, %
L				62	65	4			
М	127	125	-1	96	95	-1	97	110	+13
R				64	65	1	32	30	-6
			At sample	e station	5 m (µ	g/m ³)			
L				64	70	9	32	35	9
М	33	37	10	95	102	7	64	55	-14
R	31	32	3	32	37	21	32	28	-12
			At sample	station	10 m (µ	(g/m^3)			
L				64	65	1			
М	61	52	-17	95	85	-10	64	58	-9
R							65	60	-7

Table 1. Comparison between the simulated results (SR, $\mu g/m^3$) and the experimental results (ER, $\mu g/m^3$).



c. DPM concentration at 10 m downstream of the vehicle.

3.2. Stage 2: DPM and ventilation air flow in opposite directions (counter-flow)

Figure 8 shows the results of the CFD simulations in isometric view when DPM and air flow are in the opposite directions (counter-flow). Near LHD, a high DPM concertation can be observed in the middle of the gallery and above LHD. At the downstream side of LHD, the DPM particles spread throughout the gallery with the maximum concentration in the middle and at the sides of the gallery.

Figure 9 shows the DPM concentration at 2 m, 5 m, and 8 m downstream of the vehicle rear end. Figure 9 (a) shows a high DPM concentration near the top and bottom portions of the vehicle. Figure 9 (b) shows the maximum concentration at the top and bottom portions of the vehicle; the concentrations also spread at the left and right sides of the roadways. The DPM concentration at the LHD operator is $125 \ \mu g/m^3$. Figure 9 (c) shows the DPM flow moving towards the roof and bottom of the roadway, and the DPM concentration spreads towards the left and right sides of the roadway. Figure 10 shows the DPM concentration field at 6 m, 10 m, and 20 m downstream of the vehicle. Figure 10 (a) shows the DPM concentration at 6 m downstream of the vehicle. Here, a high DPM concentration is observed near the floor of the roadway, and the concentration gradually reduces towards the roof. Figure 10 (b) shows the DPM concentration field at 10 m downstream of the vehicle. Here, the maximum concentration is at middle of the gallery and the left and right sides of the roadways. Figure 10 (c) shows the DPM concertation field at 20 m downstream of the vehicle. Here, DPM was found to spread throughout the entire roadway. The DPM concentration at the center of the roadway was 34 $\mu g/m^3$, and similar concentrations were observed at the left and right sides of the roadway.

Table 2 shows the compared field and simulation DPM concentration results at the downstream side of the vehicle at different sampling points. In this table, it could be observed that the simulated results were in a fair agreement with the measured data; the difference varies between -21% and +21%.

%

Sample point	ER	SR	Difference,
2 m to source (a)	-	125	-
2 m to source (b)	70	55	-21
5 m to source (c)	56	60	7
5 m to source (d)	55	43	-21
8 m to source (e)	42	35	-16
8 m to source (f)	27	27	0
6 m to vehicle (g)	14	17	21
6 m to vehicle (h)	42	48	14
6 m to vehicle (i)	26	25	-3
10 m to vehicle (j)	42	48	14
20 m to vehicle (k)	28	34	21



Figure 8. DPM flow pattern-isometric view.



a. DPM concentration at 2 m downstream of the smoke pipe.





DPM concentration (g/m³)



c. DPM concentration at 8 m downstream of the smoke pipe.

b. DPM concentration at 5m downstream of the smoke pipe

Figure 9. DPM concentration at 2 m, 5 m, and 10 m downstream of the smoke pipe.



b. DPM concentration at 10 m downstream of the vehicle.

Figure 10. EC concentration at 2 m, 5 m, and 10 m downstream of the vehicle.

3.3. Changes of DPM concentration with intake air velocities

The DPM concentration at the downstream side of the vehicle may change with intake air velocities. To study this, the simulation studies were conducted with 1 m/s, 2 m/s, 3 m/s, and 4 m/s air velocities for both PDM and intake in the same direction case (co-flow). Figures 11 and 12 show the DPM concentration patterns for different intake air velocities. At a low air velocity (1 m/s), the high DPM concentration of 600 μ g/m³ was observed at a distance of 1 m from the source. The DPM concentration was reduced with increase in the ventilation air velocity. With a ventilation air velocity of 1 m/s, at 10 m downstream to the source, most of the DPM was seen to move towards the roadway walls so that the concentration at the middle of the roadway was

low. For a ventilation air velocity of 4 m/s, most of the DPM migrated towards the middle of the roadway. Figure 12 shows the DPM concentration for different air velocities at the middle of the roadway at different distances from the source. For the ventilation air velocities ranging from 2 m/s to 4 m/s, the DPM concentration decreased with increase in the air velocity. Specifically, for the ventilation air velocities of 2 m/s, 3 m/s, and 4 m/s, the DPM concentration at 50 m downstream of the vehicle was 39 μ g/m³, 23 μ g/m³, and 19 μ g/m³, respectively. If the air velocity was low (1 m/s), the very high DPM concentration of 600 μ g/m³ was observed near the source.



a. Air velocity, 1 m/s.

b. Air velocity, 4 m/s.





Figure 12. Changes in the DPM concertation with different intake air velocities.

3.4. Changes of DPM concentration with DPM temperature at smoke pipe discharge point for both co-flow and counter-flow

The DPM temperature at the smoke pipe discharge point varies with the vehicle condition, and is mainly influenced by the diesel oxidizing catalyst, diesel particulate filter, exhaust cooler, and engine load [22]. The DPM concentration and flow pattern downstream of the vehicle may depend on the DPM temperature at the discharge point. To study the effect of temperature on the DPM flow patterns, the CFD simulations were carried out, assuming the DPM source temperatures of 30 °C, 40 °C, 50 °C, and 60 °C for both the co-flow and counter-flow cases.

Figures 13 and 14 show the DPM concentrations for different DPM discharge temperatures at the source with the ventilation air in co-flow. If the temperature was high, DPM was found to disperse throughout the entire roadway. For the DPM source temperatures of 30 °C, 40 °C, 50 °C, and 60 °C, the DPM concentration at 50 m downstream to the source, middle of the roadway, and at 1.2 m height was 43 μ g/m³, 39 μ g/m³, 12 μ g/m³, and 9

 μ g/m³, respectively. Figure 15 shows the DPM flow pattern with the source DPM and ventilation air in counter-flow. In this case, the DPM dispersion does not appear to follow any particular trend due to the highly turbulent flow of the DPM particles near LHD.



Figure 13. DPM concentration with 30 °C and 60 °C of DPM temperatures at discharge point, ISO view for a coflow case.



Figure 14. Changes in the DPM concentration at downstream side of LHD with different DPM temperatures at smoke pipe for co-flow case.



Figure 15. Changes in DPM concentration at downstream side of LHD with different DPM temperatures at smoke pipe for counter-flow case.

4. Conclusions

This paper presents a detailed account of the CFD simulation studies of the effects of different ventilation air flow directions on the flow patterns of DPM generated by diesel-powered vehicle exhausts. The experimental data gathered from measurements in a coal mine was used to validate the CFD models. The simulation results were in good agreement with the field measurements. The studies show that if the DPM source flow and the ventilation air co-flow (are in the same direction), DPM is confined predominantly to the middle of the roadway. If the DPM source flow and the ventilation air flow are in counter-flow (in the opposite directions), DPM spreads throughout the entire cross-section of the roadway. In this case, the vehicle operator will be more susceptible to exposure to high concentrations of DPM. At any specific location, the DPM concentration decreases with an increase in the ventilation air velocity. For co-flow for the intake air velocities of 2 m/s, 3 m/s, and 4 m/s, the DPM concentration at 50 m downstream of the vehicle was 39 μ g/m³, 23 μ g/m³, and 19 μ g/m³, respectively. If the ventilation air velocity is 1 m/s (very low), a high concentration of DPM (up to 600 $\mu g/m^3$) is observed near the source. The DPM concentration is also influenced by the DPM temperature at the source. For co-flow, for the DPM temperatures of 30 °C, 40 °C, 50 °C, and 60 °C, the DPM concentration at 50 m downstream of the source was 43 μ g/m³, 34 μ g/m³, 12 μ g/m³, and 9 μ g/m³, respectively. To the contrary, for counter-flow, the DPM patterns did not appear to follow any

discernible trend due to the highly turbulent flow of the DPM particles near the vehicle.

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الگوی جریان ذرات معلق دیزلی (DPM) ماشین بارگیری و باربری (LHD) در معادن زیرزمینی با شرایط تهویه متفاوت

R. Morla^{*}, S. Karekal and A. Godbole

School of Civil, Mining, and Environmental engineering, University of Wollongong, Australia

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* نویسنده مسئول مکاتبات: ramsiit99@gmail.com

چکیدہ:

ماشین آلات بارگیری و باربری دیزلی LHD، معمولاً در معادن زغال سنگ زیرزمینی استفاده میشوند. علی رغم منافع این ماشین آلات، مشکل اصلی آن ها تولید ذرات معلق دیزلی (DPM) به عنوان یک عامل سرطانزا است. در این پژوهش تلاش برای ساخت مدل جریان های DPM تولید شده توسط LHD ها در محیط یک معدن زغال سنگ زیرزمینی برای جریان های متفاوت DPM و جهتهای جریان متفاوت هوای ورودی انجام شده است. آزمایش های میدانی انجام شد و برای اعتبار سنجی و تهیه نقشه ی الگوی جریان DPM از مدل های شبیه سازی دینامیک سیالات محاسباتی (CFD) استفاده شد. نتایج به دست آمده نشان داد که اگر جریان DPM و هوای ورودی هم جهت باشند، جریان MPd عمدتاً محدود خواهد شد. در مقابل اگر جریان MPd و هوای ورودی غیر هم جهت باشند، جریان DPM گسترش خواهد یافت و اپراتور بیشتر در معرض غلظت بالای DPM قرار می گیرد. به طور کلی، غلظت MPd و هوای ورودی غیر هم جهت باشند، جریان DPM گسترش خواهد یافت و اپراتور بیشتر در معرض غلظت بالای MPd قرار می گیرد. به طور کلی، غلظت MPd با افزایش سرعت هوای ورودی کاهش می باید. برای جریان های هم جهت، برای سرعت های هوای ورودی از ۲، ۳ و ۴ متر بر ثانیه، غلظت MPd در ۵۰ متری پایین دست ماشین از ۳۹ میکرو گرم بر می می بد. برای جریان های هم جهت، برای سرعت های هوای ورودی از ۲، ۳ و ۴ متر بر ثانیه، غلظت MPd در ۵۰ متری پایین دست ماشین از ۳۹ میکرو گرم بر می متر مکعب ب ه تر تیب ب ۳۹ و ۱۹ میکرو گرم بر متر مکعب کاهش می یاب.د. غلظ TMD در ۵۰ متری پایین دست ماشین از ۹۹ میکرو گرم بر می می در برای دماهای MPd از ۲۰، ۲۰، ۵۰ و ۶۰ در ۶۰ متری پایین دست منبع به تر تیب برابر ۳۴، ۳۰، ۱۲ و ۹ میکرو گرم بر می می می کاهش می یابد.

کلمات کلیدی: معادن زغالسنگ، ذرات معلق دیزلی (DPM)، ماشین بارگیری و باربری LHD دیزلی، شبیهسازی دینامیک سیالات محاسباتی (CFD).